



EFFECT of C₃-ALCOHOLS IMPURITIES on ALUMINA CATALYZED DEHYDRATION of BIOETHANOL to ETHYLENE. EXPERIMENTAL STUDY and PROCESS MODELING



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Bioethanol produced from non-food phytogetic feedstock can be used to produce ethylene as a platform product for a large number of downstream derivatives.

After distillation, bioethanol contains impurities of C₃-alcohols, which can have an adverse impact on its further processing.

Present work focused on the studies of the organic impurities influence on the dehydration of contaminated ethanol to ethylene and the catalytic activity of the proprietary alumina catalyst.

Catalyst: proprietary acid modified alumina¹⁻²

Experiment:

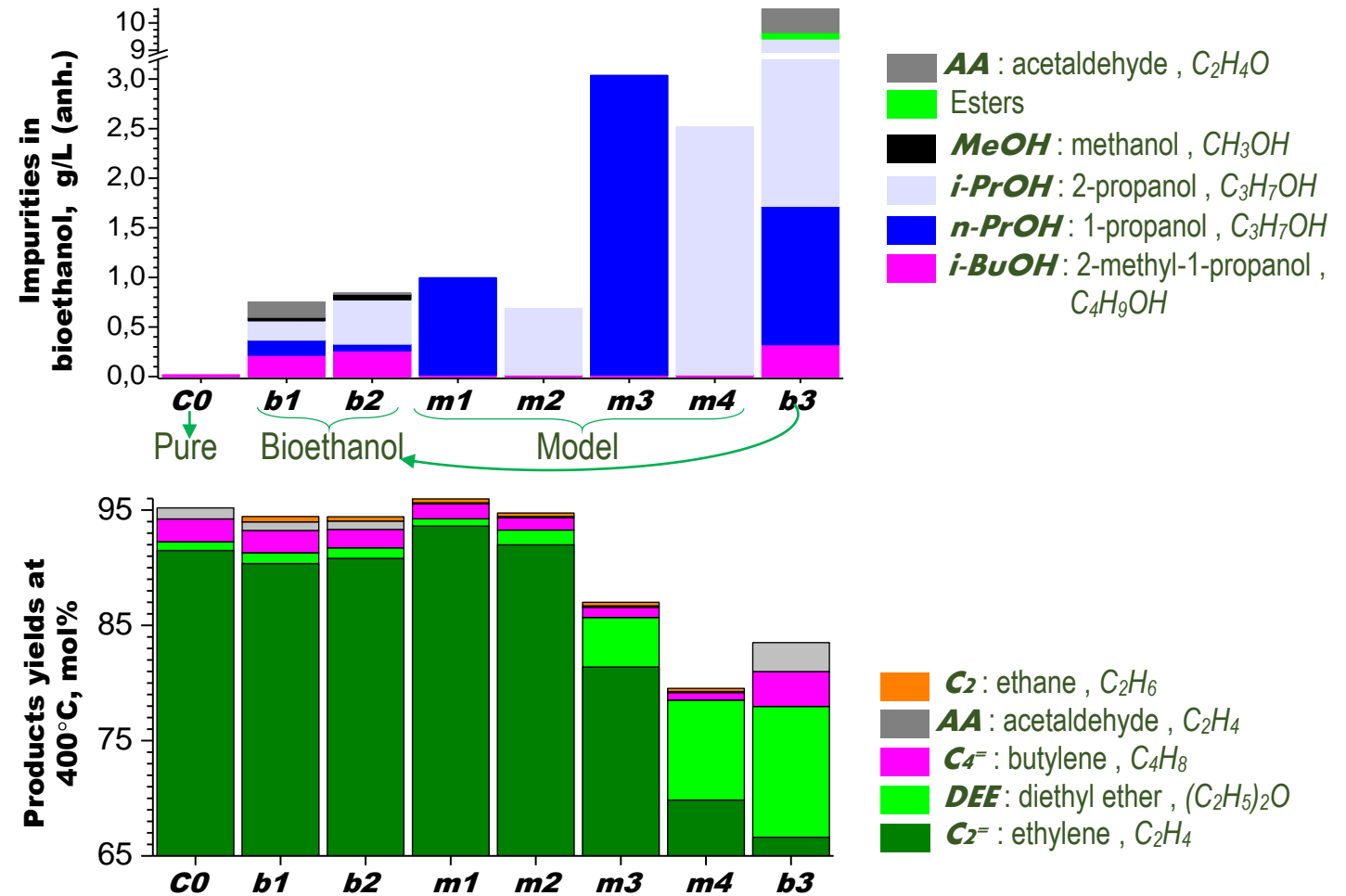
Catalyst loading: 1 ml, 6 mm ring crushed to 0.25-0.5 mm particles

Reactor: flow type

EtOH: 92%wt strength,

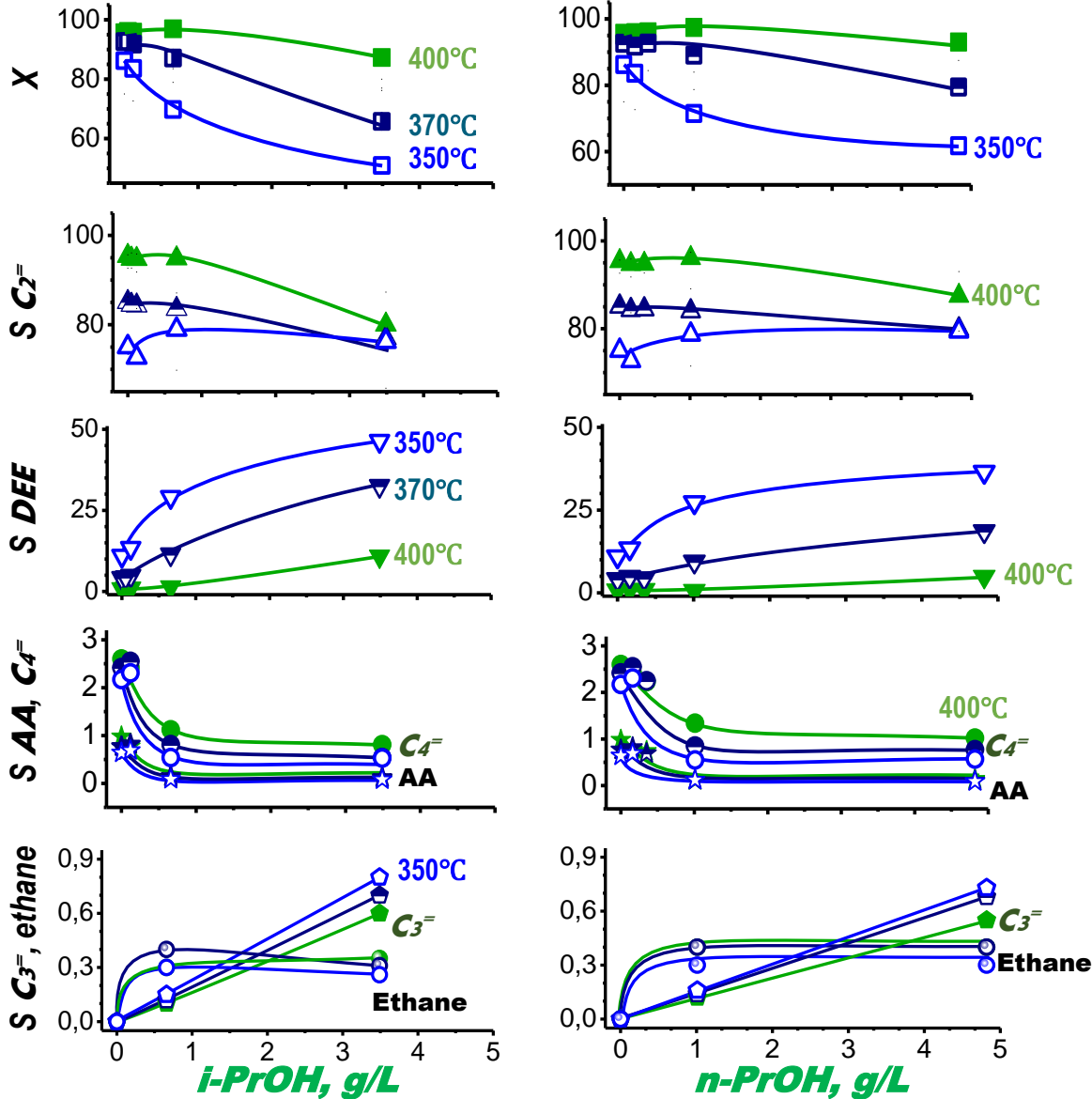
WHSV: 21 g_{EtOH} g_{cat}⁻¹ h⁻¹

T: 350-400°C



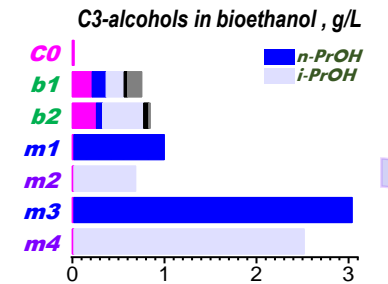
⁽¹⁾ Chem. Eng. J. 374 (2019) 605–618; <https://doi.org/10.1016/j.cesj.2019.05.149>

⁽²⁾ Russ. J. Appl. Chem. 89 (2016) 683–689; <https://doi.org/10.1134/S1070427216050013>

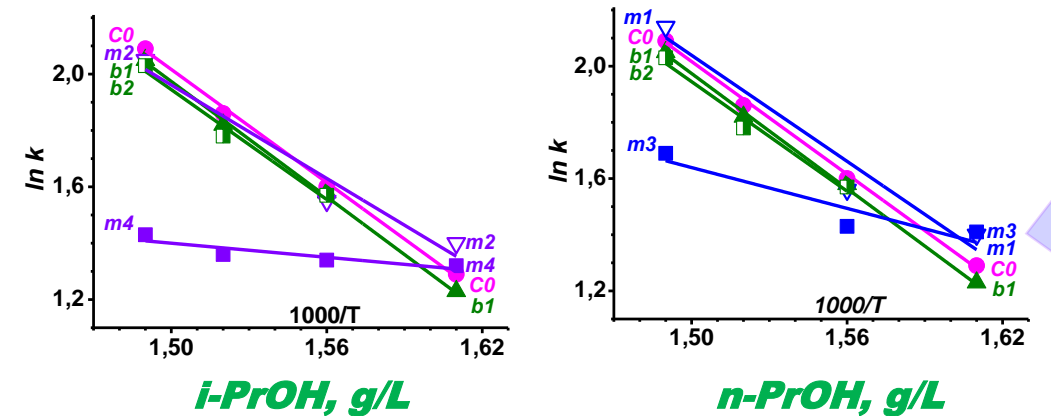


The effect of C₃-alcohols on ethanol conversion (*X*) and products selectivity (*S*, mol%) in bioethanol dehydration at 350, 370 and 400°C

C₂= (ethylene)
 DEE diethyl ether
 AA acetaldehyde
 C₄= butylene
 C₃= propylene

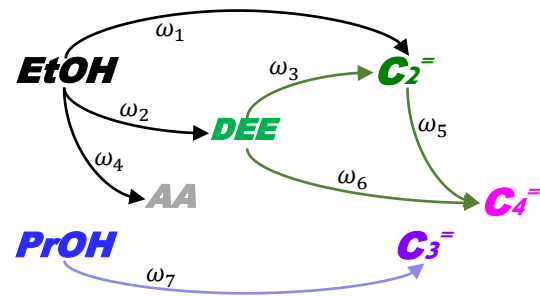


Catalyst activity in dehydration of various bioethanol samples containing C₃-alcohols



Kinetic model

Reaction network:



Kinetic equations:

$$\omega_1 = k_1 P_{EtOH} \frac{(1 + k_8 P_{PrOH})}{(1 + k_9 P_{PrOH})^2}$$

$$\omega_2 = k_2 P_{EtOH}^2 \frac{(1 + k_{10} P_{PrOH})}{(1 + k_{11} P_{PrOH})^2}$$

$$\omega_3 = k_3 P_{DEE} \frac{1}{(1 + k_{12} P_{PrOH})}$$

$$\omega_4 = k_4 P_{EtOH} \frac{1}{(1 + k_{13} P_{PrOH})}$$

$$\omega_5 = k_5 P_{C_2^=} \frac{1}{(1 + k_{14} P_{PrOH})}$$

$$\omega_6 = k_6 P_{DEE} \frac{1}{(1 + k_{15} P_{PrOH})}$$

$$\omega_7 = k_7 P_{PrOH}$$

Model of the tubular fixed-bed reactor*

*Chem. Eng. Res. Des. 145 (2019) 1-11; <https://doi.org/10.1016/j.cherd.2019.02.041>

Model of the pellet:

$$\frac{\partial}{\partial \rho} (D_{ni}^* \frac{\partial C_i}{\partial \rho}) - \frac{RT}{P} \frac{\partial}{\partial \rho} (V_i^* C_i) = \sum_{j=1}^7 \gamma_{ij} \omega_j$$

Model of the tube:

Mass and heat balance equations:

$$\frac{P_0}{RT_0} \frac{\partial (\bar{u}_l y_i)}{\partial l} + \frac{1}{r} \frac{P_0}{RT_0} \frac{\partial}{\partial r} (r \bar{u}_r y_i) - \frac{1}{r} \frac{\partial}{\partial r} (r \frac{PD_r}{RT} \frac{\partial y_i}{\partial r}) = \sum_j (1 - \varepsilon) \gamma_{ij} \omega_j$$

$$\frac{P_0}{RT_0} \bar{u}_l c_p \frac{\partial T}{\partial l} + \frac{P_0}{RT_0} \bar{u}_r c_p \frac{\partial T}{\partial r} - \sum_i c_{pi} (\frac{\partial T}{\partial r}) \frac{P}{RT} D_r \frac{\partial y_i}{\partial r} - \frac{1}{r} \frac{\partial}{\partial r} (r \lambda_r \frac{\partial T}{\partial r}) = -(1 - \varepsilon) \sum_j \Delta H_j \omega_j$$

Boundary conditions:

$$0 \leq r \leq R_{tube}$$

$$l = 0; \bar{u}_i(0, r) = \bar{u}_0; T(0, r) = T_{in}$$

$$y_i(0, r) = y_{in}$$

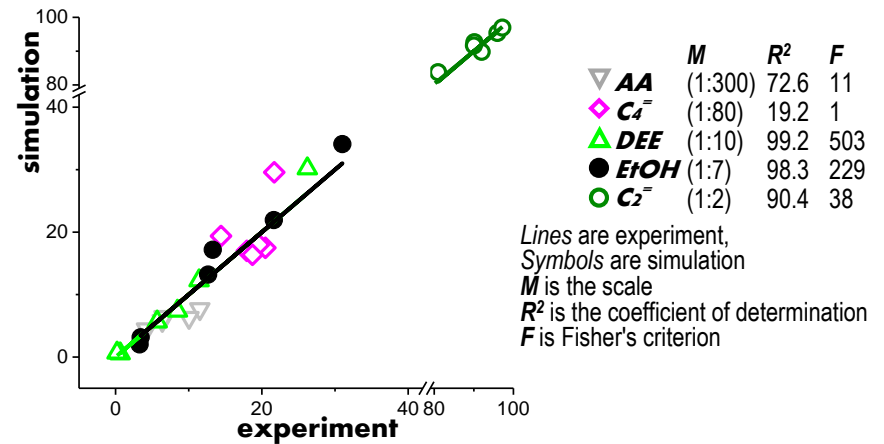
$$0 \leq l \leq L$$

$$r = 0; \frac{\partial y_i(l, 0)}{\partial r} = 0; \frac{\partial T(l, 0)}{\partial r} = 0$$

$$r = R_{tube}; \frac{\partial y_i(l, R_{tube})}{\partial r} = 0$$

$$\bar{u}_r(l, R_{tube}) = 0; \lambda_r \frac{\partial T}{\partial r} = \alpha_w (T_w - T)$$

Correlation btw simulated and measured concentrations at the reactor outlet



Conclusions

- ✓ Effect of C₃-alcohols contaminated EtOH on the catalytic dehydration to C₂H₄ was studied
- ✓ Simulation data of EtOH dehydration using a pseudo-homogeneous 2D reactor model and a draft kinetic model agreed satisfactorily with experimental results
- ✓ If the content of C₃-alcohols is less than 1.0 g/L, it affords a high yield of C₂H₄ and improves C₂H₄ quality due to a prohibited formation of by-products (C₄⁼, AA, H₂)
- ✓ To verify and confirm the preliminary results, a further in-depth study of the effect of impurities, with an expanded list and composition of components, is required.